μ(I) rheology for granular flows with *Gerris* applications for avalanches and column collapse

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outline



- what is a granular fluid? some images
- the µ(l) friction law obtained from experiments and discrete simulation
- the viscosity associated to the $\mu(I)$ friction law
- the Saint Venant Savage Hutter Hyperbolic model
- implementing the $\mu(I)$ friction law in Navier Stokes
- Examples of flows: focusing on the granular column collapse (limits of Saint Venant Savage Hutter Hyperbolic model)



- What is a granular media?
- size > 100µm
- grains of sand, small rocks, glass beads, animal feed pellet, medicines, cereals, wheat, sugar, rice...
- 50 % of the traded products

1. Introduction



IG. 1.2 - Les milieux granulaires forment une famille extrêmement vaste.

















Staron



Environmental Modelling & Software xx (2006) 1e18 www.elsevier.com/locate/envsoft

The effect of the earth pressure coefficients on the runout of granular material Marina Pirulli a,*, Marie-Odile Bristeau b, Anne Mangeney c, Claudio Scavia









Lofoten Norway



8

photo PYL





<u>http://books.google.fr/books?id=HY6Z5od4-E4C&pg=PA49&dq=granular</u> +flow&hl=fr&ei=lamtTaa_NYyVOoToldcL&sa=X&oi=book_result&ct=result&resnum=10&ved=0CFkQ6AEwCTgK#v=onepage&q&f=true





Granular Column Collapse



http://www.mylot.com/w/photokeywords/pail.asp

The sand pit problem: quickly remove the bucket of sand



The sand pit problem: quickly remove the bucket of sand





Granular Column Collapse



A possible experimental set up is a container filled by sand (left), the aspect ratio (height/length) is *a*. At initial time, the gate is opened quickly. After the avalanche, the grains stop, the final configuration is at rest (right). We compare results from Discrete Contact Method Simulations (simulation of the displacement of each grain) to a continuum Navier Stokes simulation with the $\mu(I)$ rheology *Gerrís*.

The sand pit problem: quickly remove the bucket of sand

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grains

impacts: suspension

granular media contacts

like a solid:

from the grains to the fluid



grains ϕ_{min} 0.5 (2D) 0.55 (3D)

 $\phi_{min} < \phi < \phi_{Max}$

 \oint_{max} 0.8 (2D) 0.65 (3D) from the grains to the fluid





continuum media hypothesis

from the grains to the fluid



- experiments on model material (glass bead, sand), rheology, images
- numerical experiments of contact dynamics (disks, polygona, spheres)

• Simple configuration: shear/ inclined plane



$$m\frac{d}{dt}\vec{U} = \vec{F} + \vec{F}_n + \vec{F}_t$$
 Newton's equations
branch a spring -dashpot
$$F_n = -k\delta - \gamma \frac{d\delta}{dt}$$
$$t + \Delta t$$

tangential Coulombic Friction $F_t < \mu F_n$



Contact Dynamics de (Moreau 1988) rigid grains coefficient of friction µ

$$m\frac{d}{dt}\overrightarrow{U} = \overrightarrow{F}$$

Newton's equations





Contact Dynamics de (Moreau 1988) rigid grains coefficient of friction µ

 $m(\overrightarrow{U}^+ - \overrightarrow{U}^-) = \overrightarrow{F} \delta t$ Newton's equations

take the form of an equality between the change of momenta and the average impulse during δt .

written for each grain at the contact

 u_n, u_t







- Looking for a continuum description
- Lot of recent experiments
- Simulations with Contact Dynamics



GDR MiDi EPJ E 04

Fig. 1. The six configurations of granular flows: (a) plane shear, (b) annular shear, (c) vertical-chute flows, (d) inclined plane, (e) heap flow, (f) rotating drum.



- Looking for a continuum description
- Lot of recent experiments
- Simulations with Contact Dynamics

- Defining a «viscosity»
- Implement it in the Navier Stokes solver Gerrís
- Test on exact «Bagnold» avalanche solution
- Test on granular collapse







constitutive law?





 $T = \mu N$

Coulomb dry friction Coulomb friction law

$$\tau = \mu P$$





V(z)



 $T = \mu N$

Coulomb friction law



$$\tau = \mu(I)P$$

non dimensional number: «Froude» local «Inertial Number» (Da Cruz 04-05)





 $md^2y/dt^2 = Pd^2$



 $\oint t^2 = \rho d^2 / (P)$

 $\frac{dx}{dt} = d\frac{\partial u}{\partial y} \qquad t = 1/\frac{\partial u}{\partial y}$

 $\label{eq:falling_time} \begin{array}{l} \mbox{falling time} & I = \frac{d \frac{\partial u}{\partial y}}{\sqrt{P/\rho}} \\ \mbox{displacement time} & \end{array}$

P



Da Cruz PRE 05

Coulomb friction law $\tau = \mu(I)P$

falling time displacement time

$$I = \frac{d\frac{\partial u}{\partial y}}{\sqrt{P/\rho}}$$

Pouliquen 99 Pouliquen Forterre JSM 06 Da Cruz 04-05 GDR Midi 04 Josserand Lagrée Lhuillier 04



Coulomb friction law $\tau = \mu(I)P$ $I = \frac{d\frac{\partial u}{\partial y}}{\sqrt{P/\rho}} \mu_{2}$ $\mu_{1} \simeq 0.32 \quad (\mu_{2} - \mu_{1}) \simeq 0.23 \quad I_{0} \simeq 0.3 \quad \mu_{1}$ (c) kinetic regime $\mu_{2} = \frac{d\frac{\partial u}{\partial y}}{\sqrt{P/\rho}} \mu_{2}$ (c) kinetic regime $\mu_{1} \simeq 0.32 \quad (\mu_{2} - \mu_{1}) \simeq 0.23 \quad I_{0} \simeq 0.3 \quad \mu_{1}$ (c) kinetic regime $\mu_{2} = \frac{d\frac{\partial u}{\partial y}}{\sqrt{P/\rho}} \mu_{2}$ (c) kinetic regime $\mu_{2} = \frac{d\frac{\partial u}{\partial y}}{\sqrt{P/\rho}} \mu_{2}$ (c) kinetic regime $\mu_{1} \simeq 0.32 \quad (\mu_{2} - \mu_{1}) \simeq 0.23 \quad I_{0} \simeq 0.3 \quad \mu_{1}$ (c) kinetic regime $\mu_{1} \simeq 0.32 \quad (\mu_{2} - \mu_{1}) \simeq 0.23 \quad I_{0} \simeq 0.3 \quad \mu_{1}$ (c) kinetic regime $\mu_{2} = \frac{d\frac{\partial u}{\partial y}}{\sqrt{P/\rho}} \mu_{2}$ (c) kinetic regime (c) kin





u(y)

Coulomb friction law $\tau = \mu(I)P$ $I = \frac{d\frac{\partial u}{\partial y}}{\sqrt{P/\rho}}$ «Drucker-Prager» plastic flow

equivalent viscosity

$$\eta \frac{\partial u}{\partial y} = \mu(I)p \quad \to \quad \eta = \frac{\mu(I)p}{\frac{\partial u}{\partial y}}$$



implementation in Navier Stokes?

Jop Forterre Pouliquen 2005

$$\mu(I) = \mu_1 + \frac{\mu_2 - \mu_1}{I_0/I + 1}$$
$$D_2 = \sqrt{D_{ij}D_{ij}} \qquad D_{ij} = \frac{u_{i,j} + u_{j,i}}{2}$$

construction of a viscosity based on the D_2 invariant and redefinition of I

$$I = d\sqrt{2}D_2/\sqrt{(|p|/\rho)}.$$

$$\eta = \left(\frac{\mu(I)}{\sqrt{2}D_2}p\right)$$

«Drucker-Prager»

$$\nabla \cdot \mathbf{u} = 0, \ \rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \nabla \cdot (2\eta \mathbf{D}) + \rho g,$$

Boundary Conditions: no slip and P=0 at the interface



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Saint-Venant Savage Hutter



 $\varepsilon = H/L$

 $U_0 = \sqrt{gH}.$

$$p = -\rho g \cos \alpha (\eta(x,t) - y)$$
 $\tau_{xy} = \rho g H \sin \alpha \bar{\tau}_{xy}$

$$\rho U_0^2 / L \quad \longleftarrow \quad -\frac{\partial p}{\partial x} = -\rho g \frac{\partial \eta}{\partial x}$$
$$\rho U_0^2 / (H/\varepsilon) = \rho g \varepsilon.$$



Saint-Venant Savage Hutter





Saint-Venant Savage Hutter

 $\frac{h}{h} + \frac{\partial(Q)}{\partial x} = 0 \quad \frac{\partial Q}{\partial t} + \frac{\partial}{\partial x} \left(\frac{5Q^2}{4h} + \frac{g}{2}(h^2)\right) = -gh\mu(I)\frac{Q}{|Q|}$ h

Integral over the layer of grains
Saint-Venant Savage Hutter Gerrís

$$\frac{\partial h}{\partial t} + \frac{\partial(Q)}{\partial x} = 0 \quad \frac{\partial Q}{\partial t} + \frac{\partial}{\partial x}(\frac{5Q^2}{4h} + \frac{g}{2}(h^2)) = -gh\mu(I)\frac{Q}{|Q|}$$

Gerrís is a free finite volume code by Stéphane Popinet one part of the code is a Shallow Water solver

$$\frac{Q^* - Q^n}{\Delta t} + \frac{\partial}{\partial x} \left(\frac{Q^2}{h} + \frac{g}{2}(h^2)\right) = 0 \qquad \frac{Q^{n+1} - Q^*}{\Delta t} = -gh^* \mu(I^*) \frac{Q^{n+1}}{|Q^*|}$$
Audusse et al.





valid by hypothesis for small aspect ratio









Saint-Venant Savage Hutter Gerrís





Saint-Venant Savage Hutter Gerrís











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- *Gerrís* is a finite volume code by Stéphane Popinet NIWA one part of the code is a Navier Stokes solver
- automatic mesh adaptation

H

- Volume Of Fluid method for two phase flows
- free on sourceforge



rheology; defining a viscosity

$$\mu(I) = \mu_1 + \frac{\mu_2 - \mu_1}{I_0/I + 1}$$

$$\eta \frac{\partial u}{\partial y} = \mu(I)P$$
 local equilibrium

$$\eta = \frac{\mu(\frac{d\frac{\partial u}{\partial y}}{\sqrt{P/\rho}})P}{\frac{\partial u}{\partial y}}$$

construction of a viscosity

P. Jop, Y. Forterre, O. Pouliquen, (2006) "A rheology for dense granular flows", Nature 441, pp. 727-730



implementation in *Gerrís* flow solver?

$$\mu(I) = \mu_1 + \frac{\mu_2 - \mu_1}{I_0/I + 1}$$
$$D_2 = \sqrt{D_{ij}D_{ij}} \qquad D_{ij} = \frac{u_{i,j} + u_{j,i}}{2}$$

construction of a viscosity based on the D_2 invariant and redefinition of I

$$\eta = \min(\eta_{max}, \max\left(\frac{\mu(I)}{\sqrt{2}D_2}p, 0\right)) \qquad I = d\sqrt{2}D_2/\sqrt{(|p|/\rho)}.$$

- the «min» limits viscosity to a large value
- always flow, even slow

Boundary Conditions: no slip and P=0 at the interface



implementation in *Gerrís* flow solver?

$$\mu(I) = \mu_1 + \frac{\mu_2 - \mu_1}{I_0/I + 1}$$
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$$\nabla \cdot \mathbf{u} = 0, \ \rho \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \nabla \cdot (2\eta \mathbf{D}) + \rho g,$$

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$$\frac{\partial c}{\partial t} + \nabla \cdot (c\mathbf{u}) = 0, \ \rho = c\rho_1 + (1-c)\rho_2, \ \eta = c\eta_1 + (1-c)\eta_2$$

The granular fluid is covered by a passive light fluid (it allows for a zero pressure boundary condition at the surface, bypassing an up to now difficulty which was to impose this condition on a unknown moving boundary).

Boundary Conditions: no slip and P=0 at the top





$$\frac{\partial c}{\partial t} + \nabla \cdot (c\mathbf{u}) = 0, \quad \rho = c\rho_1 + (1-c)\rho_2, \quad \eta = c\eta_1 + (1-c)\eta_2$$

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Projection Method

$$\begin{split} \rho_{n+\frac{1}{2}} \left(\frac{\mathbf{u}_* - \mathbf{u}_n}{\Delta t} + \mathbf{u}_{n+\frac{1}{2}} \cdot \boldsymbol{\nabla} \mathbf{u}_{n+\frac{1}{2}} \right) &= \boldsymbol{\nabla} \cdot \left(\eta_{n+\frac{1}{2}} \mathbf{D}_* \right) - \boldsymbol{\nabla} p_{n-\frac{1}{2}}, \\ \mathbf{u}_{n+1} &= \mathbf{u}_* - \frac{\Delta t}{\rho_{n+\frac{1}{2}}} \left(\boldsymbol{\nabla} p_{n+\frac{1}{2}} - \boldsymbol{\nabla} p_{n-\frac{1}{2}} \right), \\ \boldsymbol{\nabla} \cdot \mathbf{u}_{n+1} &= 0. \end{split}$$



multigrid solver for Laplacien of pressure

$$\boldsymbol{\nabla} \cdot \left(\frac{\Delta t}{\rho_{n+\frac{1}{2}}} \boldsymbol{\nabla} p_{n+\frac{1}{2}} \right) = \boldsymbol{\nabla} \cdot \left(\mathbf{u}_* + \frac{\Delta t}{\rho_{n+\frac{1}{2}}} \boldsymbol{\nabla} p_{n-\frac{1}{2}} \right)$$

implicit for u*

$$\frac{\rho_{n+\frac{1}{2}}}{\Delta t}\mathbf{u}_{\star} - \frac{1}{2}\nabla\cdot\left(\eta_{n+\frac{1}{2}}\nabla\mathbf{u}_{\star}\right) = \rho_{n+\frac{1}{2}}\left[\frac{\mathbf{u}_{n}}{\Delta t} - \mathbf{u}_{n+\frac{1}{2}}\cdot\nabla\mathbf{u}_{n+\frac{1}{2}}\right] - \nabla p_{n-\frac{1}{2}} + \frac{1}{2}\nabla\mathbf{u}_{n}^{T}\nabla\eta_{n+\frac{1}{2}}.$$

VOF reconstruction

$$\frac{c_{n+\frac{1}{2}} - c_{n-\frac{1}{2}}}{\Delta t} + \nabla \cdot (c_n \mathbf{u}_n) = 0$$



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TABLE 1.			
flow height Y (cm)	measured speed (cm/sec)	<pre>speed, from (9) (cm/sec)</pre>	ratio
0.5	17.2	26.4	1.53
0.65	27.5	38.8	1.41
0.75	30.0	48.0	1.6
0.9	39.0	63.0	1.61

Bagnold 1954





kind of $Nu\betaelt$ solution

Contact Dynamic simulation Lydie Staron





$$u = \frac{2}{3} I_{\alpha} \sqrt{gd \cos \alpha} \frac{H^3}{d^3} \left(1 - \left(1 - \frac{y}{H} \right)^{3/2} \right), \begin{cases} \frac{3}{2} \\ \frac{y}{2} \\ \frac{y}{2}$$





$$u = \frac{2}{3} I_{\alpha} \sqrt{gd \cos \alpha} \frac{H^3}{d^3} \left(1 - \left(1 - \frac{y}{H}\right)^{3/2} \right), \underset{S}{\oplus} \left(\frac{y}{B} \right)^{3/2} = 0, \quad p = \rho g H \left(1 - \frac{y}{H} \right) \cos \alpha.$$





$$u(y) = \frac{(2H - y)\left(\rho_f gy \sin \alpha - 2\tau_0\right)}{2\mu_f}$$

$$d\frac{\partial u}{\partial y} = \max\left[\sqrt{p_0/\rho + gH\left(1 - \frac{y}{H}\right)\cos\alpha} \times \mu^{-1}\left(\frac{\tau_0 + \rho gH\left(1 - \frac{y}{H}\right)\sin\alpha}{p_0 + \rho gH\left(1 - \frac{y}{H}\right)\cos\alpha}\right), 0\right]$$

$$u(H^{-}) - u(H^{+}) = 0$$











• Bagnold 3D



Figure 3: Typical 3D velocity profile predicted by the rheology (*W*=142d, θ =22.6°, Q/d^{3/2}g^{1/2}=15.2). For clarity only one quarter of the lines of the 71x80 computational grid is plotted.





Figure 4: Comparison of 3D simulations (lines) and experimental results (symbolism) different flow rates ($Q^*=Q/d^{3/2}g^{1/2}$). **a**, **b**, **c**, Free-surface velocity profiles for channe W=16.5d (**a**), W=140d (**b**) and W=546d (**c**). **d**, Depths of the flowing layer across the char W=140d. The experimental and computational flow rates are equal within 2.5%. The error represent the dispersion of the measurements for different experiments.

 \tilde{V}_{max} **A** \tilde{Q} **Onstitutive law for dense granular flows** Pierre Jop₁, Yoël Forterre₁ & Olivier Pouliquen

mardi 20 septembre 2011

.

 $\tilde{z} = z/W$

 $\tilde{V}_{\rm max}$





NS µ(l)



influence de la largeur sur l'écoulement: on passe de Bagnold à un écoulement en surface





profils au centre en profondeur

profils en surface vus de dessus



The sand pit problem: quickly remove the bucket of sand



Granular Column Collapse



http://www.mylot.com/w/photokeywords/pail.asp

The sand pit problem: quickly remove the bucket of sand



Collapse of columns

a=0.37



Contact Dynamic simulation Lydie Staron





Collapse of columns

a=0.90



Contact Dynamic simulation Lydie Staron







Snapshots of collapse of three columns of aspect ration 0.5 1.42 and 6.26 (top to bottom)



Collapse of columns of aspect ratio 0.5 comparison of Discrete Simulation Contact Method and Navier Stokes gerris, shape at time 0, 1, 2, 3, 4 and position of the front of the avalanche as function of time (time measured with $\sqrt{H_0/g}$ and space with aH_0)





5

NS μ(I) DCM

Collapse of columns of aspect ratio 1.42 comparison of Discrete Simulation Contact Method and Navier Stokes gerris, shape at time 0, 1, 2, 3, 4 and position of the front of the avalanche as function of time (time measured with $\sqrt{H_0/g}$ and space with aH_0)

3

2

t



DC[']M ---NS μ(I) t=0 ---NS μ(I) t=1 ---NS μ(I) t=2 ----

NS μ(I) t=3 NS μ(I) t=4

2.5

3

3.5









optimisation

$$\mu(I) = \mu_s + \frac{\Delta\mu}{\frac{I_0}{I} + 1}$$





final values

$$\mu_s = 0.32 \ \Delta \mu = 0.28 \ I_0 = 0.4$$















a = 0.5 DCM vs Gerrís $\mu(l)$












 $a = 1.42 \text{ DCM vs } Gerris \mu(l)$









a = 6.6 DCM vs Gerrís $\mu(l)$





NS/CD 1=0.0190



DCM vs Gerrís $\mu(I)$

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NS/CD L=0.0875



DCM vs Gerrís $\mu(I)$





Figure 10: Strip representing a series of snapshots (t = 0.5, 1.0, 1.2, 1.4, 1.7, and 2.0)of a column collapse with aspect ratio a = 68. The most advanced curve (in green) corresponds to $\mu_s = 0.3 \Delta m u = 0.26$ and $I_0 = 0.30$. the less advanced (in blue) $\mu_s = 0.32$ $\mu_s = 0.28$ and $I_0 = 0.30$ fits better the end of the heap. The curve in between (in cyan) corresponds to $\mu_s = 0.32 \Delta m u = 0.28$ and $I_0 = 0.40$ and fits better the top of the surge.



comparaison of velocity profiles



DCM vs Gerrís
$$\mu(I)$$



comparaison of velocity profiles





comparaison of velocity profiles





• comparaison of velocity profiles





NS/CD L=8,9318







Normalised final deposit extent as a function of aspect ratio *a*. Well-defined power law dependencies with exponents of I and 2/3 respectively.

We recover the experimental scaling [Lajeunesse et al. 04] and [Staron et al. 05]. Differences between the values of the prefactors are due to the difficulties to obtain the run out length: friction in the Navier Stokes code tends to underestimate it, whereas direct simulation shows that the tip is very gazeous, it can no longer explained by a continuum mechanic description.



conclusion

- $\mu(I)$ obtained from experimental flows of dry granular flows [Jop et al. 06], implemented it in *Gerrís*

- test case: analytical solution of steady avalanche (Bagnold solution)

- collapse of granular columns (shape as function of time compared to Discrete Simulations).

-The experimental trends of the scaling of the run out are reobtained

- Saint Venant Savage Hutter to be compared with.

- complete spectra: discrete grains/ Saint Venant/ Navier Stokes

This opens the door to systematic studies of granular flows using this continuum approach.



références:

P. Jop, Y. Forterre, O. Pouliquen, (2006) "A rheology for dense granular flows", Nature 441, pp. 727-730 (2006)

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E. Lajeunesse, A. Mangeney-Castelnau, and J.-P. Vilotte, (2004) "Spreading of a granular mass on an horizontal plane», Phys. Fluids, 16(7), 2371-2381.

L. Staron & E. J. Hinch (2005) "Study of the collapse of granular columns using two-dimensional discrete-grain simulation", J. Fluid Mech. (2005), vol. 545, pp. 1–27.